

CLAIM AMENDMENTS

1 - 44. (canceled)

1 45. (currently amended) [[A]] The method defined in
2 claim 62, further comprising the step of manufacturing a
3 ~~polyethylene terephthalate packaging web, the method comprising the~~
4 ~~steps of: feeding waste polyethylene terephthalate raw material~~
5 ~~containing dirt and without precrystallization or predrying to a~~
6 ~~twin-screw extruder at a feed rate such that flights of the~~
7 ~~extruder screws are filled only to 25% to 60% with the polyethylene~~
8 ~~terephthalate raw material while rotating the screws of the~~
9 ~~extruder at a rotation rate to plastify the material and extrude a~~
10 ~~polyethylene terephthalate melt from the extruder; degassing an~~
11 ~~interior of the extruder during the extrusion of the polyethylene~~
12 ~~terephthalate melt therefrom; passing the melt through a sieve~~
13 ~~filter and thereby separating the dirt from the melt; measuring~~
14 ~~melt pressure upstream and downstream of the sieve filter;~~
15 ~~controlling one of the rates of the extruder in accordance with the~~
16 ~~measured melt pressures;~~

17 backflushing the sieve filter with the melt and thereby
18 forcing the dirt from the sieve filter in accordance with the melt
19 pressures measured upstream and downstream of the sieve filter ;
20 ~~outputting a strip of the polyethylene terephthalate melt from a~~
21 ~~spinning head located downstream of the extruder; and cooling and~~

22 ~~stretching the strip of the polyethylene terephthalate to form the~~
23 ~~polyethylene terephthalate packaging web.~~

1 46. (currently amended) The method defined in claim
2 [[45]] 62 wherein the raw material is at least in part PET flakes
3 formed by comminuting PET bottles.

1 47. (currently amended) The method defined in claim
2 [[45]] 62 wherein the raw material is supplied to the extruder with
3 at least one metering screw.

1 48. (currently amended) The method defined in claim
2 [[45]] 62 wherein the flights of the extruder screws are filled to
3 30% to 50% with the polyethylene terephthalate raw material.

1 49. (currently amended) The method defined in claim
2 [[45]] 62 wherein the screws of the extruder are driven in the same
3 direction.

1 50. (currently amended) The method defined in claim
2 [[45]] 62 wherein the interior of the extruder is degassed by
3 connecting at least one suction pump thereto.

1 51. (canceled)

1 52. (currently amended) The method defined in claim
2 [[51]] 62 wherein the chain-lengthening substance is a lactam or an
3 oxazole derivative.

53. (canceled)

1 54. (currently amended) The method defined in claim
2 [[45]] 62 wherein the strip is cooled in a liquid.

1 55. (previously presented) The method defined in claim
2 54 wherein the liquid is a water bath.

1 56. (currently amended) The method defined in claim
2 [[45]] 62 wherein the one rate is the rotation rate.

1 57. (currently amended) The method defined in claim
2 [[45]] 62 wherein the one rate is the feed rate.

58. (canceled)

1 59. (currently amended) The method defined in claim
2 [[58]] 62, further comprising after stretching and cooling the
3 strip the step of
4 guiding the strip through a furnace and heating it
5 therein above its glass temperature.

1 60. (currently amended) The method defined in claim
2 ~~59, further comprising after stretching and cooling~~ 62 wherein the
3 strip is fixed after the first stretching step and before the
4 second stretching step by the step of again stretching the strip
5 ~~and thereafter~~
6 heating the strip in a fixing device.

1 61. (currently amended) The method defined in claim 60,
2 further comprising immediately after heating the strip in a fixing
3 device the step of
4 cooling the strip ~~and thereafter stretching the strip.~~

1 62. (new) A method of manufacturing a polyethylene
2 terephthalate packaging web, the method comprising the steps of:
3 a) feeding waste polyethylene terephthalate raw material
4 containing dirt and with no substantial pretreatment or
5 precrystallization to a twin-screw extruder at a feed rate such
6 that flights of the extruder screws are filled only to 25% to 60%
7 with the polyethylene terephthalate raw material while rotating the
8 screws of the extruder at a rotation rate to plastify the material
9 and extrude a polyethylene terephthalate melt from the extruder;
10 b) degassing an interior of the extruder during the
11 extrusion of the polyethylene terephthalate melt therefrom;

12 c) feeding at least one chain-lengthening substance to
13 the interior of the extruder for admixture with the melt;

14 d) passing the melt through a sieve filter and thereby
15 separating the dirt from the melt;

16 e) measuring melt pressure upstream and downstream of the
17 sieve filter;

18 f) controlling at least one of the rates of the extruder
19 in accordance with the measured melt pressures;

20 g) pumping the filtered polyethylene terephthalate melt
21 from the extruder to a spinning head downstream of the extruder and
22 thereby outputting a strip of the polyethylene terephthalate melt
23 from the spinning head;

24 h) cooling the strip of the polyethylene terephthalate
25 with a fluid;

26 i) twice longitudinally stretching the cooled strip; and
27 j) fixing the stretched strip to form the polyethylene
28 terephthalate packaging web.